

# Resolution of Ibuprofen with Primary Amine Carbamates in Supercritical Carbon Dioxide

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## Abstract

Three new, successful resolving agents, namely (*S*)-2-phenylglycinol, (*R*)-1-phenylethanaminium (*R*)-(1-phenylethyl) carbamate and (*S*)-2-hydroxy-1-phenylethanaminium (*S*)-(2-hydroxy-1-phenylethyl) carbamate of ibuprofen are presented. The carbamate salts are stable white crystals, they can be easily stored and handled. All salt forming resolution were performed in supercritical carbon dioxide as the only solvent. The enantioseparations were efficient (approx. 50 % enantiomeric purities, > 90 % yields in the crystalline phase) and robust. Unlike previous experiences with primary amine resolving agents, the diastereomeric salt formations and resolutions were completed in short times, even within one hour suggesting that the carbamates are intermediates of the salt formation reaction.

## Keywords

supercritical carbon dioxide, chiral, salt formation, chiral separation, carbamate, activation

## 1 Introduction

From the 1960s, importance of obtaining chiral substances in optically active form has been increasing, since the enantiomers can have different biological effects. A large share of the active pharmaceutical ingredients are chiral, thus the technologies offering enantiopure products in an economical and environmentally friendly way [1] are highly important.

Supercritical carbon dioxide is a nonpolar, non-explosive, non-toxic solvent that has a low critical temperature (31.3 °C) and acceptable critical pressure (7.31 MPa). Being a gas at atmospheric pressure, the carbon dioxide is completely removed from the product by depressurization, leaving a solvent-free product. The first use of supercritical fluid extraction for optical separation was presented by Fogassy et al. [2].

Ibuprofen is a widely applied pharmaceutical model compound, and also an active pharmaceutical ingredient. Ibuprofen is a non-steroid anti-inflammatory and analgesic compound, of which only the (*S*)-enantiomer is effective, and using pure (*S*)-enantiomer in therapy can be 3 times more effective than using the racemic form [3].

Resolution of ibuprofen as a model compound was carried out using organic solvent [4] and using supercritical carbon dioxide by supercritical fluid extraction [5, 6], by the *in situ* [7] and antisolvent [8] methods. Separation of ibuprofen enantiomers in organic solvents was carried out with numerous resolving agents such as: ephedrine [4], (*R*)-1-phenylethylamine [9], N-alkyl-D-glucamine [10] and lysine [11]. The chiral separation of ibuprofen enantiomers was also investigated by SMB (Simulated Moving Bed) [12]. As several resolutions of ibuprofen have been already developed, it is a good model substance for comparison and evaluation of novel methods.

The kinetics of the resolution of ibuprofen using (*R*)-1-phenylethylamine was investigated by Bántóczy et al. [7] by *in situ* method, it was found that the diastereomeric salt formation is a slow process, to achieve 0.422 selectivity, more than 100 hours of reaction time is needed at 20 MPa and 40 °C. It was also found that the primary amine ((*R*)-1-phenylethylamine) form carbamate with carbon dioxide, that can be detected if the reaction time is under 24 hours, but during longer reaction times it decomposes [13].

Furthermore, 1-phenylethylamine is not a very convenient resolving agent, it is a viscous liquid with a specific odor and it reacts with the CO<sub>2</sub> content of the air as well forming a solid precipitate. Its carbamate on the other hand is a stable, white solid, which allows much more convenient storing and handling.

Salt forming resolution of ibuprofen with *in situ* method with (*S*)-phenylglycinol was investigated before, but Valentine did not achieve any significant enantioseparation [14]. Despite of this, according to structural similarities [15] and differential scanning calorimetry (DSC) measurements [16], (*S*)-phenylglycinol could be a suitable resolution agent.

The aim of this work is to demonstrate novel and easy-to-apply salt forming resolutions with self-carbamate-salts of primary amines, namely of (*S*)-2-phenylglycinol and (*R*)-1-phenylethylamine, in carbon dioxide as the only solvent.

## 2 Experimental

### 2.1 Materials

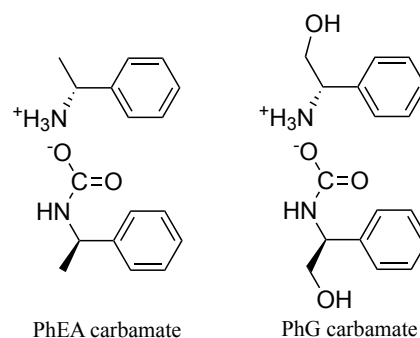
Racemic ibuprofen (IBU) ( $\geq 98\%$ ) was purchased from Tokyo Chemical Industry Ltd. (*S*)-(+)-2-phenylglycinol (PhG), CAS: 20989-17-7, ( $\geq 97\%$  GC) and (*R*)-(+)-1-phenylethylamine (PhEA), CAS: 3886-69-9, were purchased from Tokyo Chemical Industry Ltd., Carbon dioxide ( $\geq 99.5\%$ ) was purchased from Linde Gas Hungary Co., C Ltd and was used freshly distilled. Methanol was purchased from Merck Ltd.

(*R*)-1-phenylethanaminium (*R*)-(1-phenylethyl)carbamate abbreviated as PhEA carbamate and (*S*)-2-hydroxy-1-phenylethanaminium (*S*)-(2-hydroxy-1-phenylethyl)carbamate abbreviated as PhG carbamate are depicted on the left and right sides in Fig. 1, respectively. The PhEA carbamate and the PhG carbamate were produced by our high pressure vessel with pure carbon dioxide at 20 MPa, 40 °C with the reaction time of 24 h. In case of the PhEA carbamate, corresponding to previous studies pure carbamate was obtained [7]. The purity of the PhG carbamate was investigated by DSC measurements: the melting of the PhG is not detectable, thus pure PhG carbamate was obtained.

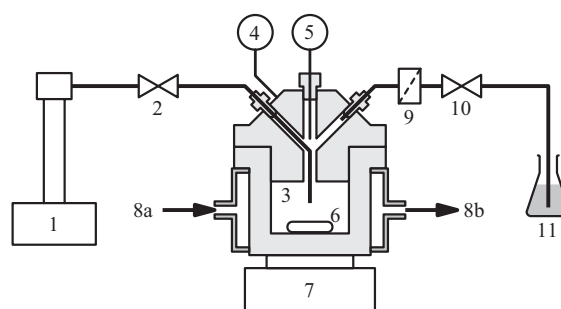
### 2.2 Equipment

A scheme of the high pressure crystallization apparatus used for the experiments is shown in Fig. 2.

The reactor was constructed by the Applied Chemistry Research Institute of Miskolc University, the inlet tube (3) was built in later to make the reactor suitable for crystallizing. The reactor is suitable to make reactions with carbon dioxide containing atmospheres at maximum 25 MPa



**Fig. 1** The structure of (*R*)-1-phenylethanaminium (*R*)-(1-phenylethyl)carbamate and (*S*)-2-hydroxy-1-phenylethanaminium (*S*)-(2-hydroxy-1-phenylethyl)carbamate)



**Fig. 2** reactor: carbon dioxide tank, pump and ISCO pump (1), inlet valve (2), inlet tube (3), pressure and temperature transmitter (4, 5), water inlet / outlet for the thermostat (8a, 8b), stirrer (6), stirring motor (7), outlet valve (10), metanol trap (11), metal filter(9)

and 100 °C (the rupture disc opens at 34 MPa). During the investigations, three reactors were used with slightly different volumes 36.4 and 37.7 ml.

The carbon dioxide was pumped into the reactor with the ISCO 260D pump through the valve (2) and the inlet tube (3). This tube is needed to ensure the carbon dioxide to flow to the bottom of the reactor, thus it cannot happen that during the washing phase not the complete volume of the reactor is washed, this would decrease the effectivity of washing.

The temperature transmitter (5) is connected to a computer in which the measured data is recorded. This way, the temperature data can be monitored any time for the entire reaction time, even days. The pressure transmitter (4) is also connected to the data recording computer and the pressure is displayed on a digital display as well.

The stirrer magnet (6) is driven by the stirrer motor (7) with up to 1100 rpm. Depressurization is possible through the outlet valve (10). In front of the valve there is a metal filter (9) to prevent crystals from flowing out of the reactor.

After washing, during depressurization the carbon dioxide was flown through trap with 40 ml methanol. This way, the extract could be collected.

The reactor's temperature was set by tempered water flown in the jacket of the reactor.

### 2.3 Methods

For all experiments 0.200 g IBU was used with 0.5 molar equivalent resolving agent which is 0.0694 g in case of using PhEA carbamate and 0.0665 g in case of PhG carbamate.

The IBU and the resolving agent were placed into the bottom of the reactor, then the reactor was closed and stirring was started at 750 rpm. The reactor was pressurized with pure carbon dioxide in 10–15 minutes. After reaching the desired pressure, the reaction mixture was continuously stirred until a pre-set time at constant pressure and temperature. Once the pre-set time elapsed, the reactor was washed with a calculated amount of CO<sub>2</sub> at constant pressure, temperature and stirring. The carbon dioxide flow rate was 1.5 ml/min and the extraction took about an hour. The extract was collected in a methanol trap. After the depressurization and the opening the reactor, the raffinate was collected in solid form. To ensure full material recovery, the part of the raffinate that could not be collected was washed out by methanol. Mass of extract and raffinate were calculated after the evaporation of the solvent. Total mass recoveries (cumulative mass of the extract and the raffinate compared to the mass of the reactants used) were excellent (95–100 %). The values above one caused by small rubber filings.

### 2.4 Determination of enantiomeric purity using capillary electrophoresis (CE)

Capillary electrophoresis measurements were carried out by Cyclolab Ltd. (Budapest, Hungary) using an Agilent Technologies (Waldbronn, Germany) <sup>3</sup>DCE apparatus, equipped with a diode array detector. All measurements were carried out using a silica capillary with untreated surface, with a total length of 58.5 cm, of which 50 cm was before the detector. The internal diameter of the capillary was 50 μm. The capillary was thermostated at 25 °C during measurements, with 20 kV voltage set between the electrodes. Analysis time was 12 min per sample. The separated components were detected at a wavelength of 200 nm. The continuously flowing electrolyte solution was a pH 4.5 Britton–Robinson buffer, with TRIMEB (permethylated-β-cyclodextrin prepared by Cyclolab Ltd.) as a chiral selector in 12.5 mM concentration. During evaluation of the electrophorograms, the percentage ratio of the peaks corresponding to the separated enantiomers compared to the cumulative area of all peaks was calculated, while the diastereomeric excess and enantiomeric excess were calculated.

### 2.5 Powder X-ray diffraction

Powder X-ray diffractograms were obtained using a PANalytical X'Pert Pro MPD (Almelo, The Netherlands) diffractometer, equipped with an X'celerator detector in Θ–Θ arrangement. The radiation source was an X-ray tube with a Cu anode, analyses were carried out at the Kα wavelength of Cu (1.5408 Å), applying 40 kV voltage and 30 mA current. The Kβ wavelength of Cu was filtered out using a nickel foil. Scanned diffraction angles were varied between 4° and 42°. The measurement time was chosen as 10 min in order to improve signal / noise ratio.

### 2.6 Calculation

The calculation methods are consistent with the earlier work of Bánsághi et al. [7] to ensure comparability.

The *F* parameter that indicates the resolution efficiency was calculated by Eq. (1)

$$F = (|ee| \cdot Y_e + |de| \cdot Y_r) / 2. \quad (1)$$

In this formula (Eq. (1)), *Y* denotes the theoretical yield, *e* and *r* subscripts denote extract and raffinate, *ee* and *de* denote enantiomeric purities of the extract and the raffinate, respectively. *F*-parameter values are in the range of 0–1. Please note, that theoretical yield is the mass of recovered material in the given fraction (i.e. extract or raffinate) relative to the theoretical mass of the given fraction assuming full conversion of the reaction and that the residence time distribution in the extraction step is according an ideal continuously stirred tank reactor (CSTR) model [7].

## 3 Results and discussion

The salt forming resolution of IBU with PhEA carbamate was investigated at 40 °C, at pressures 10–15–20 MPa and at 50 °C and 15 MPa. Fig. 3 shows the evolution of the *F* parameter values with time. The salt forming resolution is efficient with PhEA carbamate and the operational parameters do not have any significant effects. The reaction reaches an equilibrium within 24 hours in all cases and there is a similar final resolution efficiencies of *F* ~ 0.47.

Comparing the results with using the PhEA as resolving agent under the same reaction conditions [7], the equilibrium is much faster achieved (168 h → 24 h) in case of using the carbamate than using the primary amine itself.

Interestingly, the reaction starting from the PhEA carbamate seems to be the slowest at 20 MPa, while Bánsághi et al. [7] reported that increasing pressure accelerated the reaction when PhEA as primary amine was directly applied as resolving agent. The reason is supposed to be that the PhEA

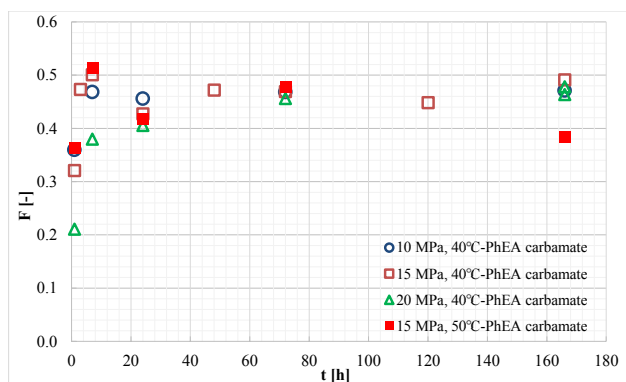


Fig. 3 Resolution of IBU with PhEA carbamate.

carbamate salt is an intermediate of the diastereomeric salt formation reaction. The first step, formation of PhEA self-carbamate salt from PhEA is faster at higher pressures. It is a carbon dioxide fixation reaction involving precipitation (volume reduction), thus not only the increasing  $\text{CO}_2$  excess by pressure, but the pressure itself. Those are both supposed to increase the reaction rates. The second step, the decomposition of the self-carbamate salt to form the diastereomeric salt with ibuprofen however, results in  $\text{CO}_2$  as byproduct, thus it should not be favored at higher pressures.

The salt forming resolutions starting from the primary amine and from its carbamate salt result in similar  $F$  values at the equilibrium, and the raffinates have similar crystal structures according to the XRD patterns (Fig. 4). The solid, crystalline raffinate do not contain significant amount PhEA carbamate, as its representative peak at  $6^\circ$  [13] is not visible in any of the diffractograms. Comparing the XRD patterns to diastereomeric salt references (atmospherically prepared and earlier obtained) peak positions and intensity ratios are similar suggesting similar solid phases.

Diastereomeric excess values in equilibrium starting from PhEA and its carbamate are similar as well,  $50\% \pm 6\%$ . Furthermore, the carbamate based reaction system is more robust. It is not sensitive to the varied process pressure and temperature.

Resolution of IBU by *in situ* diastereomeric salt formation with PhG resolving agent in pure carbon dioxide solvent was investigated at  $42.5^\circ\text{C}$  at pressures 10–15–20 MPa and at 15 MPa at different temperatures (35–42.5–50  $^\circ\text{C}$ ) as well. The formation of PhG carbamate is detectable on the XRD diffractograms at during short reaction times ( $t < 24$  h) like in case of using PhEA as resolving agent. However, in this salt forming resolution neither the pressure nor the temperature influenced significantly the reaction rate or the resolution efficiency. Thus resolution with

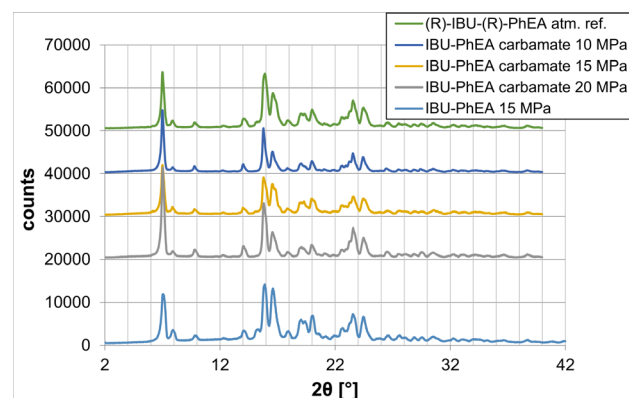


Fig. 4 Diffractograms of raffinates at  $40^\circ\text{C}$ . The green line is an atmospheric reference without  $\text{CO}_2$ .

Table 1 The detailed data of measurement results on Fig. 3.

$P$ [MPa]	$T$ [ $^\circ\text{C}$ ]	$t$ [h]	$de$ [-]	$ee$ [-]	$Y_r$ [-]	$Y_e$ [-]	$F$ [-]	recovery [-]
10	40	1	0.40	0.30	0.90	1.21	0.36	1.00
10	40	7	0.58	0.39	0.92	1.03	0.47	0.96
10	40	24	0.47	0.53	0.94	0.88	0.46	0.92
10	40	72	0.49	0.58	0.96	0.81	0.47	0.91
10	40	166	0.46	0.63	0.97	0.79	0.47	0.91
15	40	1	0.46	0.20	0.76	1.44	0.32	0.98
15	40	3	0.52	0.37	0.88	1.34	0.47	1.04
15	40	7	0.50	0.54	0.98	0.95	0.50	0.97
15	40	24	0.54	0.39	0.97	0.83	0.43	0.93
15	40	48	0.52	0.56	0.91	0.85	0.47	0.89
15	40	72	0.50	0.57	0.93	0.83	0.47	0.90
15	40	120	0.51	0.54	1.04	0.67	0.45	0.92
15	40	166	0.51	0.57	1.10	0.74	0.49	0.98
20	40	1	0.27	0.14	0.83	1.38	0.21	1.01
20	40	7	0.38	0.35	0.90	1.18	0.38	0.99
20	40	24	0.34	0.50	0.88	1.03	0.41	0.93
20	40	72	0.43	0.54	0.93	0.95	0.46	0.94
20	40	166	0.55	0.51	1.02	0.72	0.46	0.92
20	40	166	0.55	0.55	1.06	0.69	0.48	0.94
15	50	1	0.51	0.25	0.89	1.12	0.36	0.97
15	50	7	0.42	0.62	0.92	1.04	0.51	0.96
15	50	24	0.39	0.58	0.97	0.79	0.42	0.92
15	50	72	0.51	0.55	0.96	0.84	0.48	0.92
15	50	166	0.46	0.39	1.07	0.70	0.38	0.95

the PhG carbamate resolving agent was investigated at 15 MPa and  $42.5^\circ\text{C}$  only.

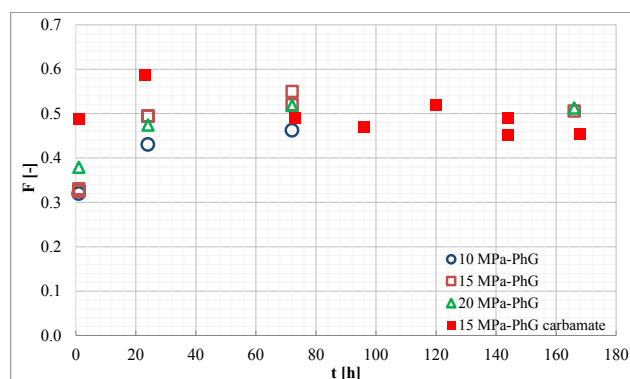
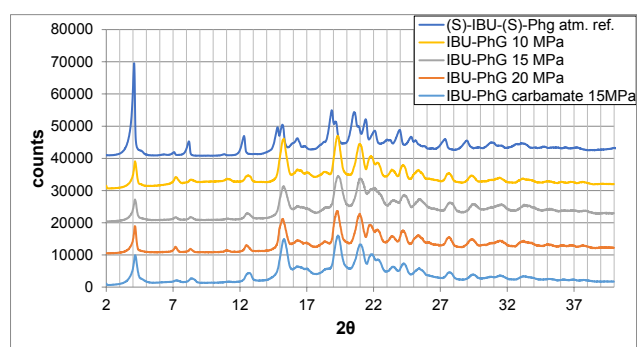
Fig. 5 shows the time scale results of the salt forming resolution of IBU with PhG and its carbamate. 24 hours are needed to reach the equilibrium, above this reaction time,  $F$  value is constant.

**Table 2** The detailed data of measurement results on Fig. 5.

$P$ [MPa]	$T$ [°C]	$t$ [h]	$de$ [-]	$ee$ [-]	$Y_r$ [-]	$Y_e$ [-]	$F$ [-]	recovery [-]
10	42.5	1	0.29	0.35	1.07	0.96	0.32	1.03
10	42.5	24	0.43	0.48	1.05	0.86	0.43	0.99
10	42.5	72	0.50	0.46	1.07	0.84	0.46	0.99
15	42.5	1	0.39	0.23	0.78	1.48	0.32	1.00
15	42.5	1	0.22	0.42	0.88	1.12	0.33	0.96
15	42.5	24	0.56	0.42	0.84	1.23	0.49	0.97
15	42.5	24	0.49	0.45	0.86	1.26	0.49	0.98
15	42.5	72	0.53	0.50	0.93	1.10	0.52	0.98
15	42.5	72	0.51	0.55	0.93	1.13	0.55	1.00
15	42.5	166	0.50	0.50	0.93	1.08	0.51	0.98
20	42.5	1	0.36	0.32	0.90	1.37	0.38	1.05
20	42.5	24	0.54	0.37	0.88	1.29	0.47	1.01
20	42.5	72	0.45	0.49	1.00	1.20	0.52	1.06
20	42.5	166	0.54	0.47	0.93	1.13	0.51	0.99
15	42.5	168	0.48	0.46	0.90	1.04	0.45	0.94
15	42.5	120	0.51	0.49	0.97	1.10	0.52	1.02
15	42.5	144	0.49	0.45	0.88	1.23	0.49	0.99
15	42.5	1	0.53	0.43	0.89	1.16	0.49	0.98
15	42.5	144	0.48	0.49	0.92	0.95	0.45	0.93
15	42.5	23	0.54	0.53	0.91	1.29	0.59	1.03
15	42.5	96	0.46	0.46	0.88	1.17	0.47	0.97
15	42.5	73	0.49	0.51	0.98	0.98	0.49	0.98

During resolution with PhG carbamate reaching the equilibrium is also faster, it was achieved in one hour. The achieved resolution is similar  $F = 0.5$ , slightly better than using PhEA resolving agent. Both PhG and PhG carbamate employing salt forming resolutions result in similar  $F$  values at the equilibrium, and the raffinates have similar crystal structures according to the XRD patterns (Fig. 6). The yield and diastereomeric excess values of the raffinates in equilibrium are  $93 \% \pm 5 \%$  and  $51 \% \pm 4 \%$ , respectively.

Further investigations are required to understand the accelerated reaction rates when the self-carbamate-salts of the primary amines are used. Taking into account that the equilibrium resolution efficiencies and diastereomeric purities are the same with the PhEA and its self-carbamate-salt and also with PhG and its self-carbamate-salt, one may assume that the carbamate is already an intermediate of the reaction. It is also possible, that the carbamates are somehow activated thus the activation energy of the diastereomeric salt formation is decreased when a carbamate is used. Sparingly, but similar observations can be found in the literature already, which makes us believe, that the self-carbamate-salts might have yet undiscovered

**Fig. 5** Resolution of IBU with PhG and PhG carbamate.**Fig. 6** Diffractograms of raffinates at 42.5 °C. The blue line is an atmospheric reference without CO<sub>2</sub>.

potentials. Nimura and coworkers published some papers in the 1980's on the analytical applications of activated carbamates [17-19] for separation of amines. Tilborg et al. [20] suggested, that natural carbonization and self-carbamate salt formation might be much common in amine involving reactions and catalysis than it was previously supposed. These forms might be more reactive than the amines themselves, which is in agreement with our experiences.

#### 4 Conclusion

Three new, successful resolving agents, namely (*S*)-2-phenylglycinol, (*R*)-1-phenylethanaminium (*R*)-(1-phenylethyl) carbamate and (*S*)-2-hydroxy-1-phenylethanaminium (*S*)-(2-hydroxy-1-phenylethyl) carbamate of ibuprofen are presented in the paper. All salt forming resolutions are efficient (appr. 50 % enantiomeric excess, > 90 % yields in the crystalline phase) and robust. The mass recovery was high, 95-100 % in most cases. The pressure and temperature, in the studied ranges, do not influence the salt forming resolution significantly. The salt forming resolution with the self-carbamate-salts of the primary amines achieve the same equilibrium in a shorter time than with the corresponding

amine suggesting an activation of the amine with its reaction with carbon dioxide forming the self-carbamate-salt. Using PhG and its derivative results in a slightly higher  $F$  value ( $F = 0.5$ ) than PhEA and its derivative ( $F = 0.47$ ).

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